Humber College of Applied Arts and Technology

Humber Lakeshore 1 Campus Master Plan Report

Appendix



Humber College of Applied Arts and Technology

Humber Lakeshore 1 Campus Master Plan Report Appendix

August 1975

Moffat Moffat & Kinoshita Architects and Planners

Accommodation Requirements at Former Lakeshore Teachers' College

Adjacent Site: View to Lake Ontario



ACCOMODATION REQUIREMENTS AT FORMER LAKESHORE	TEACHERS' COLLEGE
Registrar	Net Area (sq. ft.)
Admissions and Records Office Open Office for 4 Storage Information/Switchboard Reception/Waiting Area Test Centre (35 student station) Storage and Grading	100 250 25 50 120 600 <u>80</u>
	1225
Financial Services	
Bursar's Office Purchasing Agent's Office Open Office for 4 Stationery Storage Receiver's Office Receiving and Shipping Area	100 100 250 50 100 150
	750
Centre for Professional & Programme Developme	<u>ent</u>
Professional Development Mgr's Office Director of Academic Services's Office Secretary/Typist Open Office for 7 Equipment Storage	100 100 80 420 50 750
Administrative Office	
Principal or Dean's Office Secretary/Typist	120 80
	200
Learning Resources Management	
Learning Resources Mgr's Office	100
Learning Resources Centre	
Entrance/Circulation/Distribution Reading/Browsing/Individual Study Viewing and Listening Conference Area Office Space for 3 Workroom Stacks Magazine Storage	800 3450 150 300 300 600 <u>300</u>
	5900

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Display/Storage/Sales Manager's Office	900 100
	1000
Word Processing Centre	
3 Typing Units Storage for Paper and Supplies	160
	200
Printing Centre	
Print Room (incl. darkroom) Paper Storage Workroom for stapling/binding/collating Manager's Office	500 175 425 60
	1160
Instructional Materials Centre	
Equipment Storage and Distribution Screening Room	250 150
	400
Secretarial Studies	
1 Typing Lab for 70 3 Typing Labs for 35 1 Shorthand Lab for 40 1 General Office Machines Lab for 50 1 Office Simulation Lab for 15	1350 2325 600 1000 450 5725
Business	
5 Classrooms for 25 to 30 1 Complex Business Machines Lab for 30 Dean's Office Secretary 25 Faculty Offices @ 70 s.f	4000 750 120 80 1750
	6700
English Communications	
1 Lab for 50 3 Discussions/Seminar Rooms for 30	1350 1500
	2850

Accounting/Bookeeping	
1 Classroom for 40	1000
Mathematics	
1 Classroom for 30	750
Humanities	
2 Classrooms for 30	1500
Applied Arts	
1 Metal Arts Lab for 20 1 Travel and Tourism Classroom for 30 1 Law Enforcement Classroom for 30	1500 750 750
	3000
Placement and Counselling	
Counsellor's Office	100
Health Services	
Nurse's Office Exam Room Reception/Waiting Area 2 Sick Bays @ 100 s.f. Treatment Room 2 Washrooms @ 30 s.f. Storage	80 80 200 80 60 40
	620
Athletics	
Programme Director's Office 2 Male Locker/Toilet/Shower Areas 2 Female Locker/Toilet/Shower Areas Equipment Room- Rental Equipment Room- Storage	100 900 1100 200 150
	2450
Student Union Facilities	
Office/Workroom Recreation/Seating Area Vending Area	150 1170 <u>380</u> 1700

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Caretaking Office/Lunchroom 2 Custodial Rooms @ 100 s.f. 4 Custodial Rooms @ 25 s.f.	200 200 100
	500
Groundskeeping	
Storage (can be external to building)	200

Total Net Area of New Facilities

38,780 sq. ft.

Mechanical Appendix

Lake Ontario. View Southeast



MECHANICAL APPENDIX

GENERAL

To carry out this analysis, a building of 150,000 square feet, similar to the second phase of new construction, was used.

Since population and classroom usage vary as a function of the daytime, utilization profiles were developed from data established by the north campus of Humber College, Chart One.

This information was used to derive the combined loss/gain diagram for occupied periods, Figure Three, and also the hourly cooling profile on a peak day, Chart Three.

HEAT RECLAIM

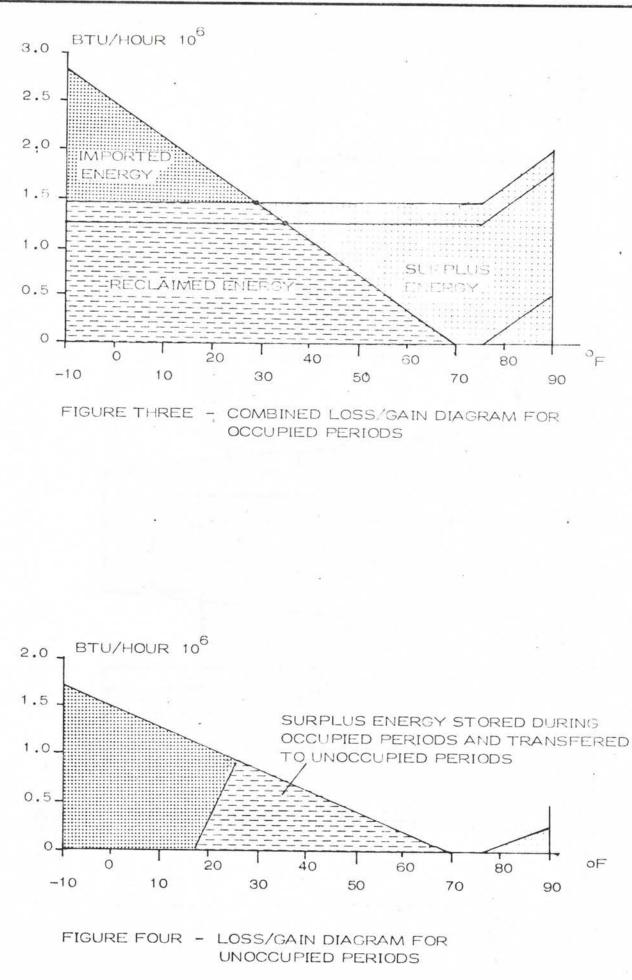
The validity for using the heat of lights, people and equipment, Figure Three, to offset fabric losses can be shown in two ways.

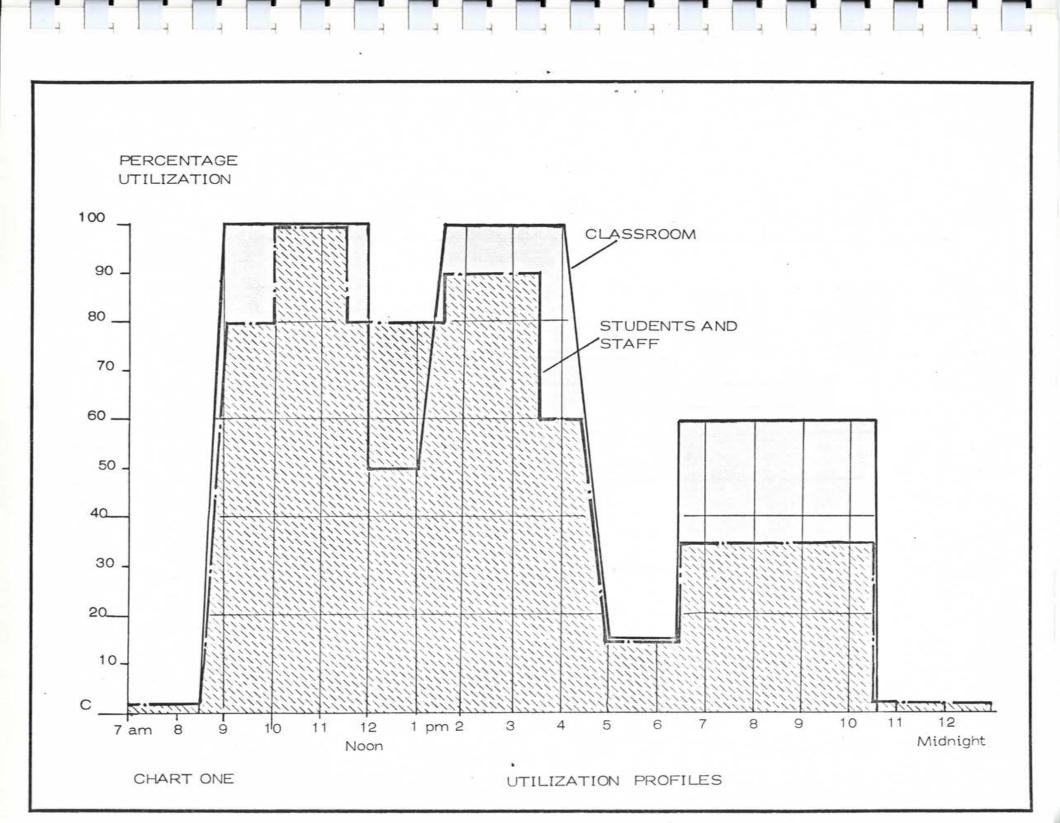
The electrical energy required to drive a heat pump to reclaim 14,730 BTU's is approximately 0.8 kilowatts. At a cost of 1.8 cents/kilowatt hour, the cost for reclaimed heat equals $\frac{0.8 \times 1.8}{14.73}$ 0.0978 cents for each 1,000 BTU/hour reclaimed.

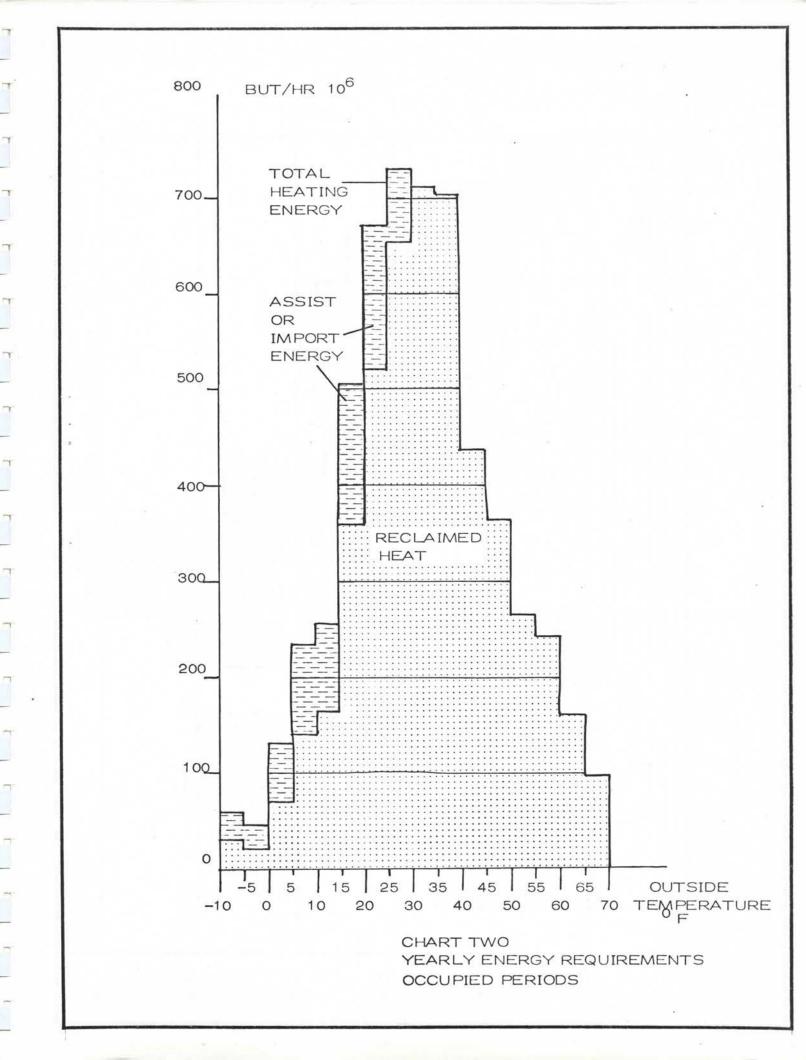
Natural gas at 125 cents for 1,000 cubic feet and 75 per cent combustion efficiency costs $\frac{125}{1,000 \times 0.75}$ 0.167 cents for each 1,000 BTU/hour.

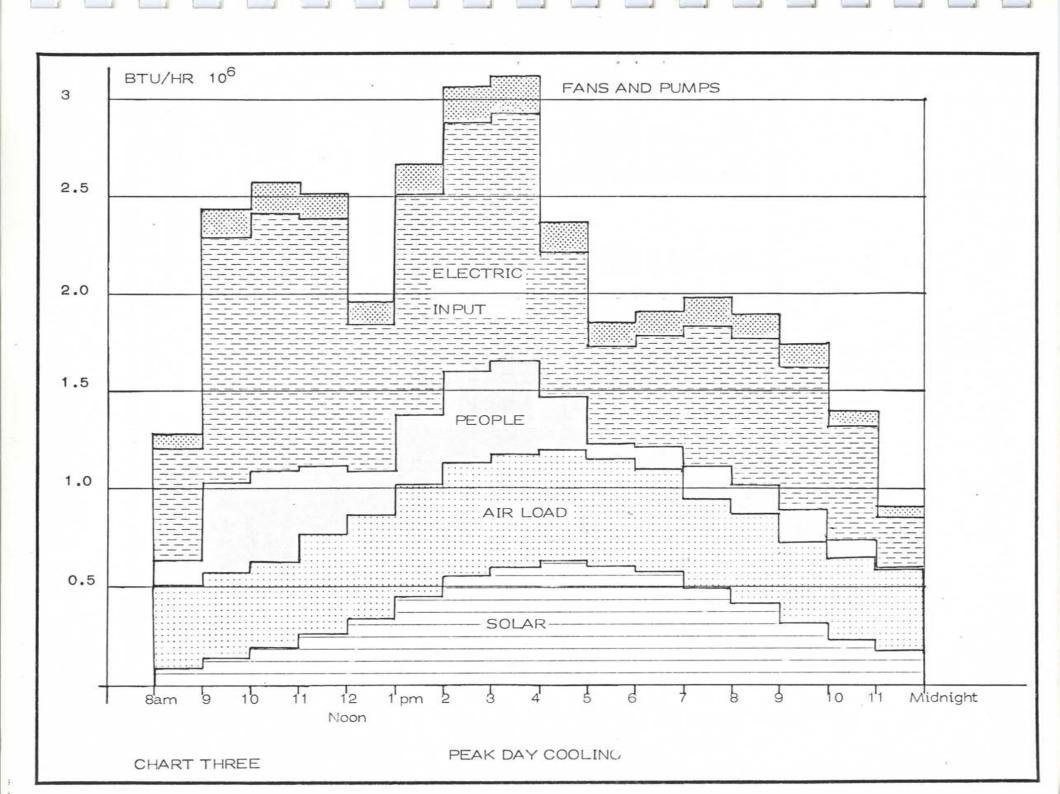
A heat pump reclaiming free heat therefore shows a saving of 42 per cent over fossil fuel.

To justify the capital expenditure of a heat pump necessary to achieve this saving, sufficient heat has to be reclaimed. This is shown on Chart









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Two and was calculated as follows:

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1.	2.	з.	4. Maximum Reclaim	5. Reclaimed Heat
		Average	Heat	Col. 2 x
		Loss	Available	Lowest Value
Temp, Band	No. Hours	BTU/hr.	BTU/hr.	of Cols. 3 or 4
-10 / -5	21	2,870,000	1,400,000	29.4 × 10^{6}
- 5/ 0	16	2,690,000	1,400,000	22.4 × 10^{6}
0/5	51	2,511,250	1,400,000	71.4×10^{6}
5/10	101	2,331,875	1,400,000	141.4×10^{6}
10/15	119	2,152,500	1,400,000	166.6×10^{6}
15 / 20	256	1,973,125	1,400,000	358.4×10^{6}
20 / 25	373	1,793,750	1,400,000	522.2×10^{6}
25 / 30	465	1,614,375	1,400,000	651×10^{6}
30 / 35	509	1,435,000	1,400,000	712.6×10^{6}
35 / 40	561	1,255,625	1,400,000	704.4×10^{6}
40 / 45	403	1,076,250	1,400,000	433.7×10^{6}
45 / 50	406	896,875	1,400,000	364.1×10^{6}
50 / 55	372	717,500	1,400,000	266.9×10^{6}
55 / 60	450	538,125	1,400,000	242.1 \times 10 ⁶
60 / 65	470	358,750	1,400,000	168.6×10^{6}
65 / 70	548	179,375	1,400,000	98.3 × 10 ⁶

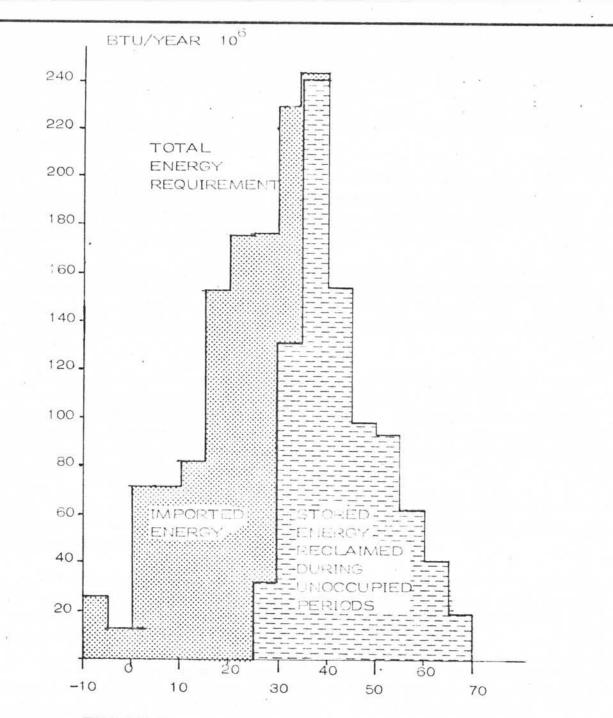
The total energy saved per year amounts to 4953.5×10^6 BTU. This saving for reclaimed heat over natural gas, translated into 1975 dollars, equals \$3,429.00.

 $\frac{4953.5 \times 10^6}{10^3} \times \frac{0.167 - 0.0978}{100}$

With the cost of reclaim equipment at \$100.00 per 15,000 BTU/hour reclaimed, the pay off period is approximately three years. Assuming energy escalates in cost 20 per cent per year, this period reduces to 2.4 years.

THERMAL STORAGE

Further energy savings can be achieved using thermal storage.





 $\sum_{\text{RECLAIMED ENERGY}} = 877 \times 10^{6} \text{ BTU/YEAR}$

In the past, storage has been discounted because of the problems of blending and transfer pumping energy.

To prevent blending of usable and return water, baffles and diaphragms may be used. In Japan, honeycomb baffles have achieved antiblending efficiencies in excess of 85 per cent. A patented diaphragm by Engineering Interface Limited eliminates blending completely.

By themselves, diaphragms or baffles are not sufficient to ensure effective use of the stored water. All useful energy of any water taken from storage must be transferred if savings are to be realized. This is achieved by maintaining the system temperature range under all operating conditions.

Excessive pumping energy can be involved when transferring water from an atmospheric tank to a pressurized system. Costs and limits of the pressurized tanks tend to dictate this route. To reduce this energy requirement, Engineering Interface Limited has, in conjunction with others, developed a pump/turbine combination to transfer the pressure energy of the return water to assist the pump motor.

The use of these components to save energy is demonstrated by Figures Four and Five. Surplus energy from occupied periods can be transferred to unoccupied periods via thermal storage.

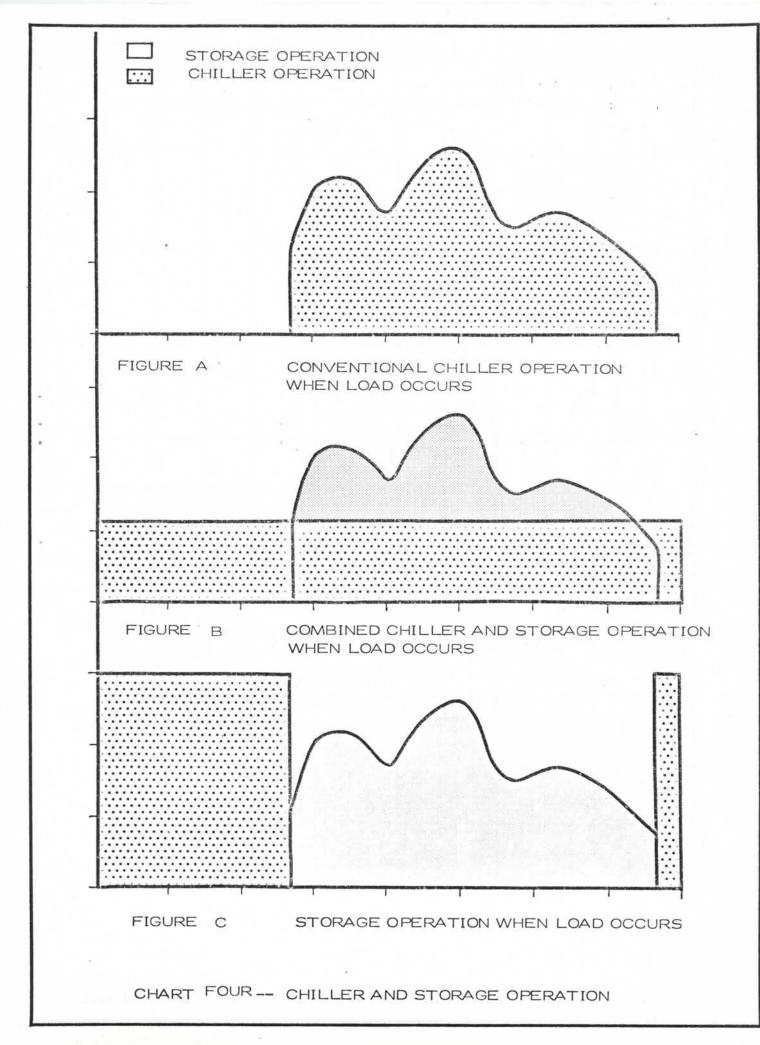
Additional savings in energy are achieved due to the normal 10°F to 20°F reduction in temperature that occurs during unoccupied night periods. This can be seen by reviewing the energy requirement at 60°F during occupied periods against 40°F during unoccupied periods.

For the chosen building, heating of 358,750 BTU/hour is required during occupied periods, whilst the heat of lights, people and equipment for reclaim amounts to 1,400,000 BTU/hour. An occupied surplus of 1,041,250 BTU/hour exists which would be lost without storage.

With storage, this can be transferred to satisfy an unoccupied heating requirement of 637,500 BTU/hour. Thus, energy is not only saved but is shifted to conditions where it can do more useful work.

The total energy saved, calculated in a manner previously indicated in this Appendix, is shown on Figure Five and amounts to 876,000,000 BTU/year. Using the 1975 dollars, the value of the saved energy amounts to $\left(\frac{876 \times 10^6}{10^3} \times \frac{0.167 - 0.0978}{10^2}\right)$ \$606, assuming the electric costs of operating the heat pump are a mix of demand and energy.

.... 4.



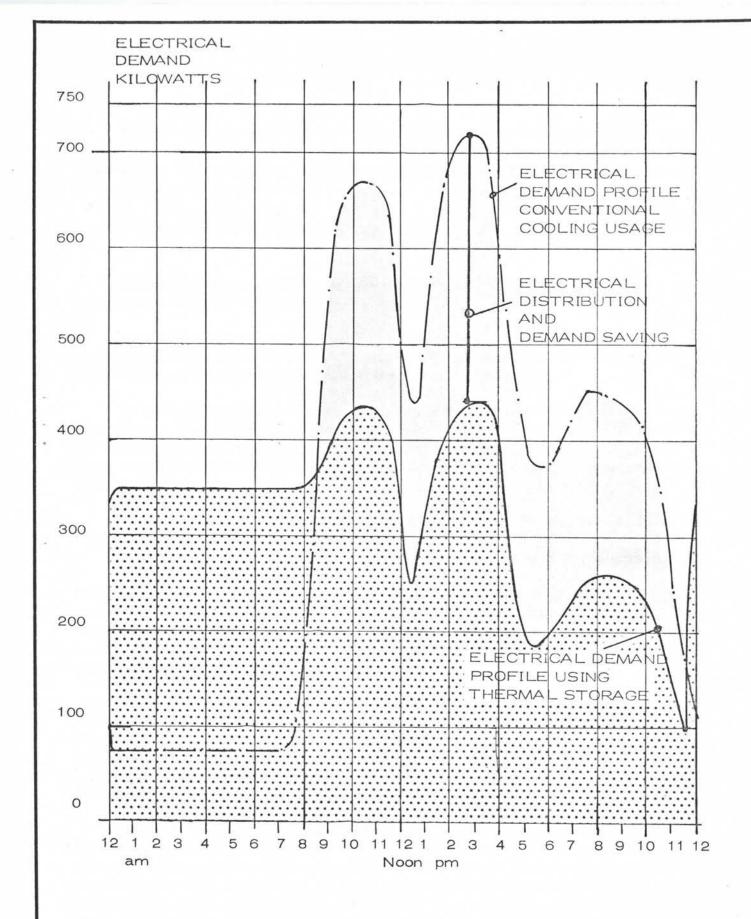


CHART FIVE ELECTRIC DEMAND PROFILES

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If, as will be shown later, the heat pump can be operated outside of demand, only electric energy costs are involved at 0.65 cents per kilowatt/hour. Thus the value of the energy saved during both occupied and unoccupied periods amounts to

 $\left[\frac{(876+4953.5)}{10^3}\times10^6\times0.167-\frac{0.65}{15}\times\frac{1}{100}\right] = $7,209.$

Without storage, costs are reduced only \$3,429. Therefore, the savings attributable to storage amount to \$3,780.

Electric demand saving using storage is best shown by considering the daily cooling requirements, Chart Three, in conjunction with the possible modes of operating the cooling equipment, Chart Four.

If the cooling load is handled in a conventional manner as in Figure A, Chart Four, the chiller electric demand occurs concurrent with the maximum building lighting and equipment electric demand. The chiller, therefore, increases the instantaneous demand and electric demand cost penalties are incurred.

These penalties can be reduced or eliminated using storage and two methods are shown on Chart Four, Figures B and C.

Figure B shows a smaller chiller combined with water storage. During unoccupied periods the chiller cools down the stored water. When cooling is required, the chiller and storage combine to satisfy the load. The smaller chiller requires less electrical input and the concurrent instantaneous maximum electrical demand of chiller, lights and equipment during occupied periods is reduced.

A further refinement is shown in Figure C, Chart Four. During unoccupied periods the chiller cools the storage water. When cooling is required, the storage alone satisfies the load. This way the instantaneous maximum electrical demand occurs either during the occupied periods as a function of the lights and equipment, or during unoccupied periods as a function of the chiller. Demand penalties are eliminated.

Chart Five identifies the electric demand profiles associated with the chiller operated in a conventional manner as in Figure A, Chart Four, and with storage as in Figure C, Chart Four. From this it can be seen that with storage, the chiller demand is totally eliminated and chiller operation is taken at base energy rates. If this principle is also applied when using the heat pump, that is the storage is used for heating, then

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heat energy is obtained at the basic energy rate.

The cost savings for cooling using 1975 hydro rates are:

(A) Conventional chiller operation peak day. Figure A, Chart Four.

Peak demand - 714 kilowatts Total daily demand - 8,542 kilowatt hours over 22 occupied days/month

Costs:

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714 × 0.35	=	\$ 250
100 × 714 × 0.0295	=	2,106
$100 \times 714 \times 0.01$	=	714
(22 × 8542 - 200) × 0.0065	=	1,220
	4	\$4,290

Average rate - 2.28¢/kilowatt hour.

(B) Storage use during occupied periods, chiller use during unoccupied periods. Figure C, Chart Four.

Peak demand - 435 kilowatts Total daily demand - 8,205 kilowatt/hours Occupied days - 22/month

Costs:

435 × 0.35	=	\$ 152
100 × 435 × 0.0295	=	1,283
100 × 435 × 0.1	=	435
(22 × 8205 - 200) × 0.0065	=	1,172
		\$3,042

Average rate - 1.69¢/kilowatt hour.

Over the 5 months requiring cooling, total savings amount to \$5,340, allowing progressive reduction in the cooling load.

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Thus, storage can result in total savings of \$9,120 per year, resulting from \$3,780 for heating and \$5,340 for cooling. The amount of storage required to achieve this saving is determined from the peak day cooling and the intermediate heating/cooling requirements.

On the peak day, Chart Three, the total cooling required is 2,964 ton hours. With a twenty degree differential on the water, the total storage required amounts to $\frac{2,964 \times 12,000}{20 \times 8.35} \times 1.05$ 224,000 U.S. gallons.

By compartmentalizing the tank, it can be used for both heating and cooling. At intermediate conditions, when cooling and heating balance, 1,620 ton hours of cooling are required with 117,000 U.S. gallons of storage devoted to cooling. Heating and cooling balance at this intermediate condition; assuming the same temperature range, a similar amount of water should be devoted to heating storage. Thus, the total storage required at intermediate conditions amounts to 234,000 U.S. gallons.

With additional allowance for losses, approximately five per cent this becomes the design volume.

Based on the chosen building, the most desirable approach to storage is that shown by Figure Three, Chart Four.

For 250,000 U.S. gallons of storage, installation costs would be approximately:

Storage Tank	-	\$119,000
Baffle	-	18,000
Transfer Pumping	-	3,000
Controls	-	1,000
*		\$141,000

Assuming that storage is only used on the second phase of the project and the first phase chiller is used for regeneration, the cost premium for storage equals \$141,000 minus the cost of an equivalent 260 ton chiller of \$56,800, i.e., \$84,200. For cost savings of \$9,120 per year and 20 per cent escalation in energy cost rates, the write-off period is approximately 12 years.

The alternate approach of combining chiller and storage to satisfy the load would, based on similar calculation, take 18 years to write off.

Probably the best demonstration of storage is shown in a comparison

of life cycle costs developed later.

WASTE HEAT BY INCINERATION

With the adoption of thermal storage, it is possible to save further energy using a waste incinerator. The heat energy developed during pyrolysis can be reclaimed at efficiencies up to 60% and stored for use when required. Additionally, the waste heat can be used to provide low temperature domestic hot water.

Based on North Campus data, approximately 9,000 lbs. per week of number one waste will be generated at the Lakeshore Campus. This equals 6,480,000 BTU/day of reclaimed heat, allowing incineration six hours per day for five days.

Additional reclaim heat is available if the waste from the North Campus is trucked to Lakeshore Campus for incineration. Based on 25,000 lbs. per week, the reclaim heat would equal 18,000,000 BTU/day.

From Figure Five and Chart Two of this Appendix, it is possible to establish that 1,320,109,200 BTU are required per year as assist energy.

For the temperature range that heat is required for assist energy, approximately 65 days are available for incineration. Thus 1,170,000,000 BTU's are reclaimed and a \$1,950 fuel saving is realized.

 $\frac{1,170,000,000}{750,000}$ $\times\,1.25$. Additionally, dumping costs are saved at North

and Lakeshore Campuses for three months at a total cost of \$900. Trucking of waste to Lakeshore Campus would cost approximately \$270, allowing 33 days of 30 miles per day and 27 cents per mile. Therefore, the total savings for incineration would equal \$2,580 (1,950 + 900 - 270).

With the cost of incineration at \$98,000, the write-off period equals 20 years, assuming escalation at 20 per cent per year. Savings in energy make this system worthy of consideration; costs, however, show no gain since the average life expectancy of incineration equipment is also 20 years.

SOLAR HEATING

Whenever there is a requirement for heating and solar gain exists,

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advantage should be taken of this energy.

This is only possible if individual room control is provided on the heating system. If such turn-down capability is not provided, the gain will be additive to internal gains of lights and people. Despite reclaim through a heat pump, this will involve additional use of motors and hence, energy waste.

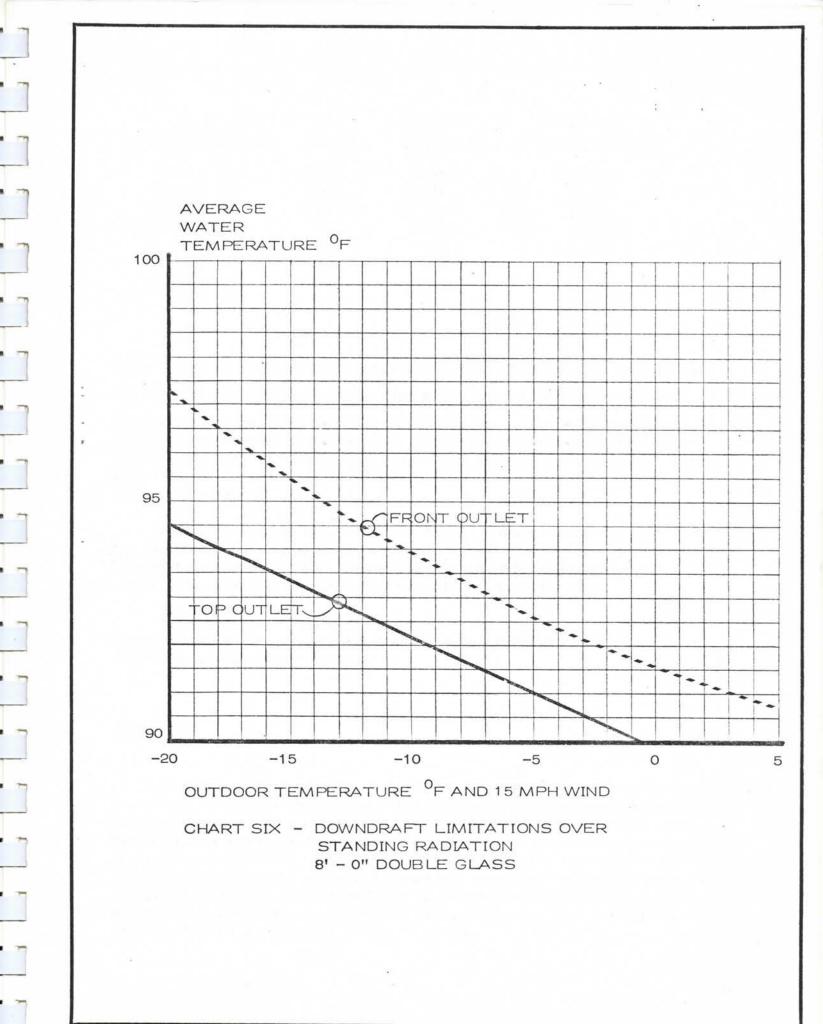
Solar collection is difficult to predict in view of the lack of information on cloud duration at the various outside temperatures. Assuming average solar data are worthy of consideration, together with average cloud cover, then the following average solar heat would be collected each hour related to all twenty-four hours of the day:

Month	Average BTU/hour, sq.ft. of collector related to 24 hours	
January	19.1	
February	22.8	
March	20.9	
April	16.5	
May	12.8	
June	12.4	
September	27.0	
October	26.8	
November	24.0	
December	21.6	

Allowing the maximum gain occurs at 70° F and the minimum at -10° F with linear variation between, the following amount of solar heat could be collected by one square foot of collector each year:

Temp. Band	Hours	Average Collection	BTU/Year sq.ft. Collector
-10 / -5	36	13.6	489
-5 / 0	24	14.7	353
0/ 5	100	15.6	1,560
5 / 10	152	16.5	2,508
10 / 15	184	17.3	3,183
15 / 20	387	18.2	7,043
20 / 25	538	19.1	10,276
25 / 30	650	20	13,000

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Temp. Band	Hours	Average Collection	BTU/Year sq.ft. Collector
30 / 35	269	20.9	5,622
35 / 40	333	21.8	7,260
40 / 45	240	22.7	5,448
45 / 50	184	23.6	4,342
50 / 55	220	24.5	5,390
55 / 60	193	25.4	4,902
60 / 65	195	26.3	5,128
65 / 70	184	27.0	4,968
			81,470

Assuming this replaces gas energy at 125¢ per 750,000 BTU useful heat, the savings using this collected solar energy equal $\frac{81,470}{750,000} \times 125 = 13.5$ cents per year for each square foot of collector. Based on a collector of decking with channels, double glass and insulation, the costs per square foot of collector, including piping, would be approximately \$6.00. Thus, the write-off period would be 21 years, assuming fuel escalation at 20 per cent annually.

Allowing 30 year collector life, this is not unreasonable; however, too many unknowns have to be resolved. Cloud duration has to be established, together with solar intensities related to temperature ranges, and useful collection has to be equated to building requirements.

In view of the viability of storage, it would seem worthwhile providing a pilot solar collection system on this campus to determine these data by suitable measurement.

SYSTEMS

In keeping with heat reclaim, the heating equipment should be sized to suit the maximum temperature that can be achieved off the heat pump. Based on low pressure machines, the most efficient operation for combined cooling and heating applications is obtained using a maximum water temperature of 105° F. At this temperature the motor horsepower per ton is not significantly increased above that required for cooling only. In any case, as can be seen from Chart Six, the maximum temperature required for a 4¼" square finned tubed element beneath 8 ft. high double glass is 104° F, assuming a twenty $^{\circ}$ F range.

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Air/water systems are compatible with heat reclaim and are most suitable to multiple perimeter spaces. On this project the ventilation requirements may preclude air/water systems in view of the penalty applied by increasing air quantities. In any case, all-air systems, in view of their application to both internal and perimeter spaces, show greater adaptability. This is particularly true when considering variable air volume all-air systems.

Multiple control and heat reclaim is possible, together with savings in energy. This is best demonstrated by comparing energy budgets of a variable air volume system against a change-over air/water system for the perimeter 20 feet spaces and air reheat system for all internal spaces. The manual derivation of these budgets is shown on following pages. Computer techniques can also be used. To maintain simplicity of procedure, thermal storage has been ignored. Its impact would, however, be of almost equal magnitude and would not affect the relationship between system budgets.

ENERGY BUDGETS

Energy Budget - Internal Spaces

Gain per square foot, based on gross area.

	Room S.H.	Return Air S.H.	<u>L.H.</u>
Lights	3.36	1.62	
Equipment	0.78		
People	.86		0.71
5	5.00	1.62	0.71

 $20^{\circ} F \Delta T = 0.23 \text{ cfm/square foot.}$

Air mixtures with outside air mixed to provide free cooling or heat reclaim:

Summer Cycle

O.A. $87^{\circ}FDB \quad 75^{\circ}FWB$ Minimum O.A. based on gross area - 0.06 cfm/square foot Room $76^{\circ}FDB \quad 50\%$ RH

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Return air temperature rise
$$\frac{1.62}{.23 \times 1.08} = 6.5^{\circ}F$$

Thus, return air temperature = 82.5° F DB

^oF DB mix =
$$\frac{.06}{.23} \times 87 + \frac{.17}{.23} \times 82.5$$

= 22.7 + 61 = 83.7^oF DB

M.C. gain =
$$\frac{.71}{.23 \times .68}$$
 = 4.5 grains/lb.

From a psychometric chart allowing 2° F supply fan gain and coil by-pass factor of 0.05 - off cooling coil = 54° F DB, 96% RH and the actual room condition is maintained at 78°F DB, 48% RH.

Total heat transferred = 8.95 BTU/lb.

=	4.5 × 8.95 × .23
=	9.26 BTU/hour, sq.ft.
=	1.08 × .23 × (83.7 - 54)
=	7.38 BTU/hour, sq.ft.
	=

Intermediate Cycle

Outside air 76^oF DB, 48% RH No perimeter heating required Maximum free cooling

Total heat transferred = 7.0 BTU/lb.

Total heat/sq.ft. = $4.5 \times 7.0 \times .23$ = 7.25 BTU/hour, sq.ft. Sensible heat/sq.ft. = $1.08 \times .23 \times (76 - 54)$ = 5.46 BTU/hour, sq.ft.

Intermediate Cycle

Outside air 50°F DB, 50°F WB.

Perimeter loss/square foot gross area - 2.83 BTU/hour, square foot.

False cooling load required to achieve this heating = $2.83 \times .81 = 2.30$ BTU/hour, sq.ft.

Related to 0.23 cfm/sq.ft., this equals 2.23 BTU/lb.

From a psychometric chart, the required mix conditions to achieve this false cooling = 60.8° F DB, 71% RH.

Total heat transferred = 2.3 BTU/hour, sq.ft.

Sensible heat = $1.08 \times .23 \times (60.8 - 54)$ = 1.69 BTU/hour, sq.ft.

Winter Cycle

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Outside air 30°F DB (Balance Point)

Perimeter loss/sq.ft. gross area - 5.68 BTU/hour.

Outside air load = $.06 \times 1.08 \times (76 - 30) = 2.98$

. . Total Gain available = 7.33 BTU/hour, sq.ft.

Heat Pump heat = $\frac{7.33 - 2.98}{.81}$ = 5.4 BTU/sq.ft., close enough to the above perimeter loss/sq.ft., based on initial graphical solution.

Related to 0.23 cfm/sq.ft. this equals 5.22 BTU/lb.

From a psychometric chart, the required mix conditions to achieve the necessary false cooling = 74° F DB, 21% RH.

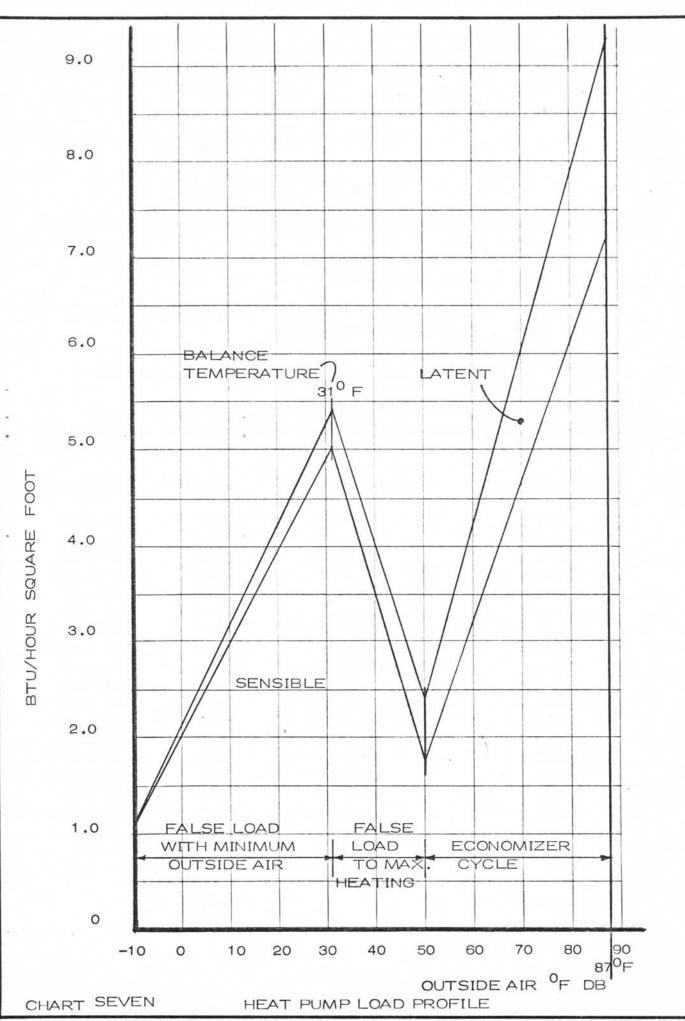
Total heat	=	5.40 BTU/hr., sq.ft.
Sensible heat	=	1.08 × .23 × (74 - 54)
	=	4.97 BTU/hr., sq.ft.

Winter Cycle

Outside air -10°F DB saturated.

N.B. - In order to obtain maximum reclaim false cooling load, minimum outside air is maintained below balance point.





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Thus ^oF DB mix =
$$\frac{.06}{.23} \times -10 + \frac{.17}{.23} \times 82.5$$

= -2.6 + 61
= 58.4^oF.

Since the off coil condition = 54° F DB, total heat transferred = 1.7 BTU/lb.

Total heat/sq.ft.	4.5 x .23 x 1.05 1.09 BTU/hour, sq.ft.
Sensible heat/sq.ft.	1.08 × .23 × (58.4 - 54) 1.09 BTU/hour, sq.ft.

The above data, in graphical form, are shown on Chart Seven.

The actual operating hours in 5 degree bands multiplied by the average heat pump load for that band in BTU/hour, square foot, establishes the equipment load per year.

Temp. Band	Hours	BTU/hr.,sq.ft.	BTU/sq.ft.,yr.
90 / 85	60	9.26	555.6
85 / 80	176	9.0	1,584
80 / 75	364	8.1	2,948.4
75 / 70	463	7.15	3,310.5
70 / 65	548	6.2	3,397.6
65 / 60	470	5.25	2,467.5
60 / 55	450	4.25	1,912.5
55 / 50	372	3.25	1,209
50 / 45	406	3.15	1,278.5
45 / 40	403	3.9	1,571.7
40 / 35	561	4.75	2,664.8
35 / 30	509	5.35	2,723.1
30 / 25	465	5.30	2,464.5
25 / 20	373	4.76	1,775.5
20 / 15	256	4.25	1,088
15 / 10	119	3.75	446.3
10 / 5	101	3.25	328.3
5/0	51	2.70	137.7
0/-5	16	2.15	334.4
-5 / -10	21	1.65	34.6

6,184

31,932.5

Energy Requirements of Equipment

Refrigeration

Design Tons $\frac{9.26}{12,000}$ = .00077 tons/sq.ft. 0.8 kilowatt/ton

Cooling Tower

0.045 Kilowatt/ton

Condenser Water Pumps

3 USGPM/ton, 60 foot head, 70% efficiency

Pump Kw = $\frac{3 \times 60 \times .746}{3,960 \times .7}$ = 0.05 Kw/ton

Chilled Water Pumps

1.2 USGPM/ton, 80 foot head, 70% efficiency

Pump Kw = $\frac{1.2 \times 80 \times .746}{3,960 \times .7}$ = 0.026 Kw/ton

Fans

1.0 cfm, 3.5 inches w.g., 64% efficiency

 $\frac{1.0 \times 3.5 \times .746}{6,350 \times .64} = 0.0006 \text{ Kw/cfm}$

@ 0.23 cfm/sq.ft. = 0.00014 Kw/sq.ft.

Equipment Loads

Refrigeration 0.8 Kw/ton

Auxiliaries (.045 + .05 + .026) .00077 + .00014

= 0.000233 Kw/sq.ft.

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Refrigeration tons/sq.ft., year = $\frac{31,932.5}{12,000}$ = 2.66

Refrigeration KWH/sq.ft., year = $2.66 \times 0.8 = 2.13$

Auxiliaries $6,184 \times 0.000233 = 1.44$

Total energy for internal spaces = 3.57 KWH/sq.ft., year, based on gross area.

Energy Budget Perimeter Spaces

Walls glazed on north and south aspects.

Areas		Transmission/ ⁰ F		
N Glass	6,720	4,368		
S Glass	6,720	4,368		
N Wall	6,720	1,008		
S Wall	6,720	1,008		
E Wall	13,440	2,016		
W Wall	13,440	2,016		
Roof	58,800	5,880		
Floor	58,800	588		

21,252

Gross building area - 150,000 sq.ft. Glass shading factor - 0.60

Transmission loads BTU/hr., sq.ft. related to gross area

 $=\frac{21,252}{150,000}=0.142$

Outside 87°F DB Room 76°F DB

Transmission = $0.142 \times 11 = 1,562 \text{ BTU/hr.,sq.ft.}$

Outside 76°F DB Room 76°F DB

Transmission = 0

Outside 70°F DB Room 70°F DB

Transmission = 0

Outside -10°F DB Room 70°F

Transmission = $0.142 \times 80 = 11.36 \text{ BTU/hr.,sq.ft.}$

Time-averaged Solar Factors for the operating hours between 8:00 a.m. and 11:00 p.m., derived from six hour ASHRAE averaged solar heat gain factors.

January	<u>N</u>	S	Total
8:00 a.m.	2	39	41
9:00 a.m.	6	90	96
10:00 a.m.	:0	133	143
11:00 a.m.	12	169	181
Noon	14	198	212
1:00 p.m.	16	217	233
2:00 p.m.	16	218	234
3:00 p.m.	14	196	210
4:00 p.m.	11	147	158

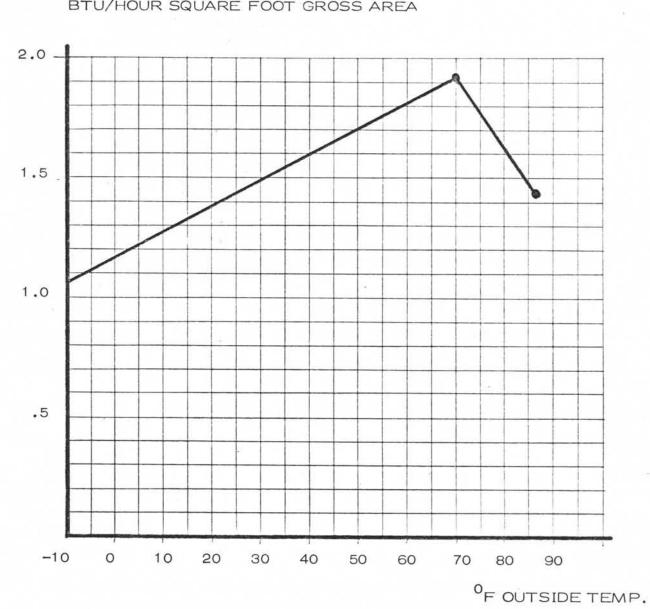
1,508

Averaged and weighted factor -

 $\frac{1,508}{2 \times 16} = 47 \text{ BTU/hr.,sq.ft. glass}$

Based on similar calculations -

51 BTU/hr.,sq.ft. glass
45 BTU/hr.,sq.ft. glass
38 BTU/hr.,sq.ft. glass
33 BTU/hr.,sq.ft. glass
33 BTU/hr.,sq.ft. glass
34 BTU/hr.,sq.ft. glass
37 BTU/hr.,sq.ft. glass
45 BTU/hr.,sq.ft. glass
50 BTU/hr., sq.ft. glass
46 BTU/hr.,sq.ft. glass
45 BTU/hr.,sq.ft. glass



BTU/HOUR SQUARE FOOT GROSS AREA

CHART NO. EIGHT AVERAGE BLOCK SOLAR LOAD

Average block solar gain BTU/hr., sq.ft. gross area -

January	$\frac{47 \times 6,720 \times 2}{150,000} \times 0.6 \times 0.42 (\% \text{ sun}) = 1.06$
February	1.32 BTU/hr.,sq.ft.
March	1.26 BTU/hr.,sq.ft.
April .	1.18 BTU/hr.,sq.ft.
May	1.10 BTU/hr., sq.ft.
June	1.21 BTU/hr.,sq.ft.
July	1.35 BTU/hr.,sq.ft.
August	1.43 BTU/hr.,sq.ft.
September	1.50 BTU/hr.,sq.ft.
October	1.56 BTU/hr.,sq.ft.
November	1.92 BTU/hr.,sq.ft.
December	1.16 BTU/hr.,sq.ft.

These values are profiled on Chart Eight.

Net loss/gain and air modulation as a result of perimeter solar and transmission therefore equals:

Outside temperature	87	80	76	70	60	50	31	-10
Transmission	1.56	. 57	0	0	-1.42	-2.84	-5.54	-11.36
Solar	1.43	1.62	1.78	1.92	1.80	1.70	1.50	1.06
Net gain/loss	2.99	2.19	1.78	1.92	.38	-1.14	-4.04	10.30
Average Perimeter air cooling 20 ⁰ F	.14	.1	.08	.09	.02			
diff. cfm/sq.ft.								

Since this air is additional to that required to cool the internal gains, the associated cooling load required is that necessary to cool from room conditions to supply conditions plus any fan gains, i.e., $76^{\circ}F$ DB, 50% RH to $54^{\circ}F$ DB, 96% RH. Cooling load = 8.9 BTU/lb. of air.

Obviously, where the gain condition occurs at outside conditions below those maintained in the space, free cooling is used to reduce the refrigeration load, i.e., at 70° F outside cooling load = 5.1 BTU/lb.; 65° F outside cooling load = 3.6 BTU/lb., and 60° F outside cooling load = 2.2 BTU/lb.

Temp.	Operating	BTU/hr.	BTU/year
Band	Hours	gross sq.ft.	gross sq.ft.
87 / 85	60	5.61	336.6
85 / 80	176	4.81	846.6
80 / 75	364	4.01	1,459.6
75 / 70	463	3.06	1,416.8
70 /65	548	2.07	1,134.4
65 / 60	470	0.89	418
60 / 55	450	0.20	90
	2,531		5,702.0

Thus cooling load BTU/hr., sq.ft. equals BTU/lb. air x cfm/sq.ft. x 4.5.

Tons/gross sq.ft. = $\frac{5,702}{12,000}$ = 0.475

KWH/ton of refrigeration - 0.8

KWH/gross sq.ft. = $0.475 \times 0.8 = 0.38$

Maximum tons/sq.ft. at 87°F due to perimeter

Transmission	1.56
Solar	1.99

3.55 BTU/hr., gross sq.ft.

Maximum perimeter air 20° F temperature difference = 0.16 cfm/sq.ft.

Cooling load = $8.9 \times 0.16 \times 4.5 = 6,408$

 $\frac{6,408}{12,000}$ = .000534 tons/sq.ft.

Auxiliary Energy Requirements

Cooling tower	-	.045	kilowatt/ton
Condenser pumps	-	0.05	kilowatt/ton
Chilled Water pump	-	0.026	kilowatt/ton

Total - 0.121 kilowatt/ton

.121 x .000534 = .000065 kilowatt/gross sq.ft.

$2,531 \times .000065 = 0.16 \text{ KWH/gross sq.ft.}$

Fans = 0.0006 Kw/cfm.

Thus, fan energy equals:

Temp. Band	Hours	cfm/sq.ft.	KWH/sq.ft.
Banu	Hours		<u>NVH/SQ.IC.</u>
87 / 85	60	.14	0.005
85 / 80	176	.12	0.013
80 / 75	364	.10	0.022
75 / 70	463	.08	0.022
70 / 65	548	.09	0.030
65 / 60	470	.06	0.017
60 / 55	450	.02	0.005
			0.114

Therefore, total energy requirements as a function of cooling at the perimeter equal:

-	0.38
	0.16
-	0.12
	-

0.66 KWH/gross sq.ft.

Occupied heating using a heat pump, is satisfied down to $31^{\circ}F$ DB. Below $31^{\circ}F$ DB, supplementary heating is required. From Chart Seven it is possible to determine the heat available from the heat pump in BTU/hr. gross square foot. Reducing the transmission by this amount indicates the quantity of imported heat required.

	A	В	C	A(B - C)
Temp.		Transmission	Heat Pump	3
Band	Hours	BTU/hr.,sq.ft.	BTU/hr.,sq.ft.	BTU/sq.ft.,yr.
-10/ -5	21	11.36	1.70	203
- 5/ 0	16	10.65	2.10	137
0/ 5	51	9.94	2.70	369
5/10	101	9.23	3.10	619
10/15	119	8.52	3.70	574

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	А	В	С	A(B - C)
Temp.		Transmission	Heat Pump	
Band	Hours	BTU/hr.,sq.ft.	BTU/hr.,sq.ft.	BTU/sq.ft.,yr.
15/20	256	7.81	4.20	924
20/25	373	7.10	4.70	895
25/30	465	6.39	5.30	507
				4,228

Unoccupied Heating Requirements:

Temp.		Transmission	BTU/year
Band	Hours	BTU/hr., sq.ft.	sq.ft.
-10/-5	15	11.36	170
- 5/ 0	8	10.65	85
0/ 5	29	9.94	487
5/10	51	9.23	470
10/15	65	8.52	554
15/20	131	7.81	1,023
20/25	165	7.10	1,172
25/30	185	6.39	1,182
30/35	269	5.68	1,527
35/40	333	4.97	1,655
40/45	240	4.26	1,022
45/50	184	3.55	653
50/55	220	2.84	625
55/60	193	2.13	411
60/65	195	1.42	277
65/70	184	0.71	131

11,444

Thus, total heating requirements, occupied and unoccupied periods = 15,672

$$\frac{15,672}{3,410}$$
 = 4.60 KWH/gross sq.ft.

Total number of hours when heating is required = 7,608.

Peak heating requirement = 11.36 BTU/hr., sq.ft.

Based on 20°F temperature range, 60 ft. head, 70% efficiency

Pump Kw = $\frac{11.36 \times 60 \times .746}{20 \times 500 \times 3,960 \times .7}$ = .00002 Kw/sq.ft.

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Pumping = $7,608 \times 0.00002 = 0.15 \text{ KWH/gross sq.ft.}$

Thus, total energy budget for a variable air volume system with heat pump reclaim:-

3.57 0.66 4.60 0.15

8.98 Kilowatt hours/gross square foot.

On a similar basis, an air/water changeover system with heat reclaim would have an energy budget of 10.69 Kilowatt hours/gross square foot.

LIFE CYCLE COSTS

In addition to Energy Budget comparisons, some relationship between costs also has to be developed. To provide a complete picture, the cost relationship should include elements of the first cost, annual energy, annual cost of labour, materials for upkeep, and replacements to plant as required throughout the term.

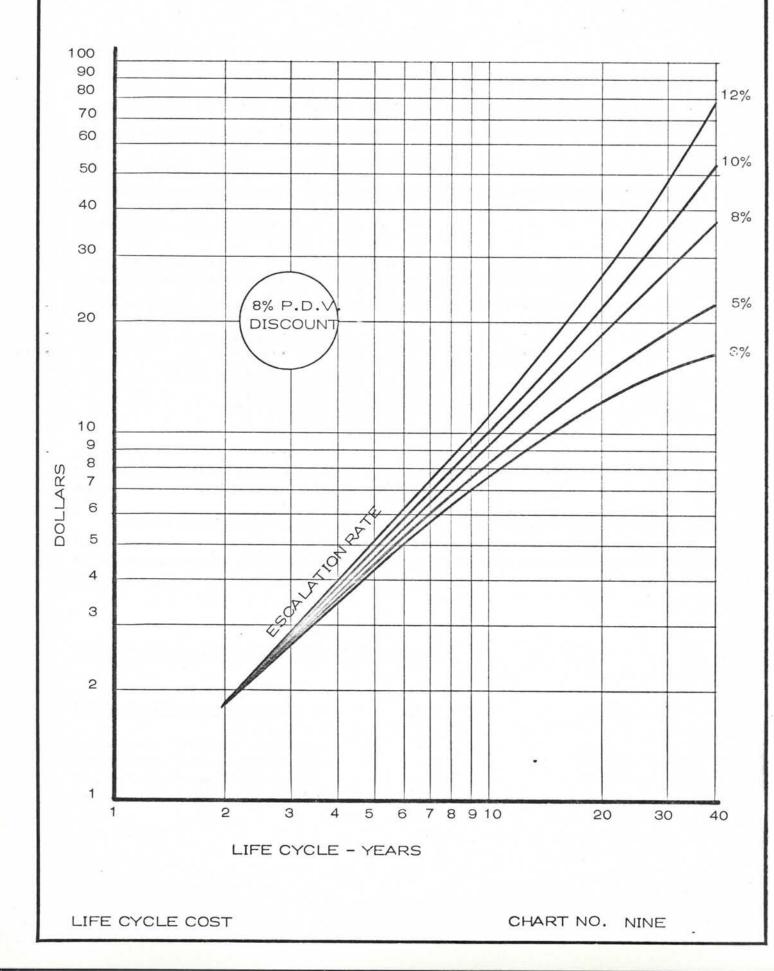
Life cycle costing offers one method of achieving this. The present day value (P.D.V.) is used as the comparator and translates future expense back to net equivalent cost at the time of the analysis.

The interest rate is expressed as P.D.V. discount. The P.D.V. is, therefore, the amount of money invested at the time of the analysis which, at the P.D.V. rate of discount, will yield enough money in the future to retire the future expense.

The value of this technique is that it permits the effects of escalation and short equipment life to be incorporated and compared. Not that anyone can predict these; rather, the sensitivity of the costs to various escalation rates and equipment life can be established.

Present Day values come in various forms. For this project, since deficit funding is not being considered, only three P.D.V.'s need be used.

Firstly, there is the cost of the initial installation. Assuming lump



sum bidding, the lump sum cost is the P.D.V.

Secondly, there is the P.D.V. of a fixed future expense. This can be established by taking the future dollars and multiplying by the equation $\frac{1}{(1+i)^n}$, where i is the interest rate and n is the number of years to the future expense. When only current dollars of the future expense are known, then the equation becomes $\frac{(1+E)^n}{(1+i)^n}$, where i and n are as before and E is the percentage escalation.

Finally, there is the P.D.V. of a recurring annual expense. This may be established by multiplying the expense in dollars by the equation $\frac{1}{i} \left[1 - \frac{1}{(1+i)^n} \right]$ where i and n are as before. When the annual expense escalates, the equation becomes

$$\frac{\left(\frac{1+E}{1+i}\right)\left[\left(\frac{1+E}{1+i}\right)^{n}-1\right]}{\left(\frac{1+E}{1+i}\right)-1}$$

Graphical solutions of this equation, related to an annual expense of one dollar, are shown on Chart Nine.

To demonstrate the use of life cycle costing, two examples follow. Firstly, central plant for this campus is compared to diversified equipment located in each new phase of construction. Secondly, the use of thermal storage against conventional equipment is compared.

LIFE CYCLE COST ONE - CENTRAL PLANT

Equipment Requirements	Cooling Tons	Heating MBH
Lakeshore Teachers' College	300	-
Phase One, New Construction	100	2,900
Phase Two, New Construction	260	2,900
Phase Three, New Construction	260	2,900
Total	920	8,700

Initial Costs

3 x 3,000 MBH boilers Gas vents Heating pumps, 600 USGPM 1,200 ft. 6" heating pipe 2 x 460 ton chillers 2 x 240 ton reclaim condensers Chilled water pumps, 1,100 USGPM Condenser water pumps, 2,760 USGPM 920 ton cooling tower 1,200 ft. 8" chilled water pipe 1,050 Kw electrical distribution Building enclosure		\$ 24,000 6,000 30,000 138,000 24,000 6,600 13,800 27,600 48,000 31,500 40,000
Total	-	\$392,500
Future Cost 1 (1975 dellars)		
Additional distribution pipework Phase Two New Construction 600 ft. 5" heating pipe 600 ft. 6" chilled water pipe	-	\$ 12,000 18,000 \$ 30,000
Future Cost 2 (1975 dollars)		
Additional distribution pipework Phase Three New Construction 300 ft. 3" heating pipe 300 ft. 4" chilled water pipe	j. I	\$ 4,500 6,000 \$ 10,500
Annual Energy Costs (1975 dollars)		
Each Phase Cooling - \$18,360 Heating - 7,970	-	\$ 26,330
Annual Labour Costs (1975 dollars)		
Four operators	-	\$ 60,000

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Annual	Maintenance	Costs	(1975	dollars)
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Clean boilers	-	\$ 500
Clean chillers	-	1,200
		\$ 1,700
Replacement Costs (1975 dollars)		
Boilers - year 20	-	\$ 24,000
Chillers - year 25	-	162,000

Life Cycle Cost - 30 Years	8% P.D.V.	Discount for	Central Equipment
Initial Costs		-	\$ 392,500
Future Costs, Phase Two (6% es 30,000 $\times \left(\frac{1.06}{1.08}\right)^2 =$	calation)	-	28,900
Future Costs, Phase Three (6% e 10,500 $\times \left(\frac{1.06}{1.08}\right)^2 =$	escalation)	-	9,750
Annual Energy Costs (10% escala	ition)		
Phase One 26,330 × 40		-	1,053,200
Phase Two 26,330 × 38 ×	$\left(\frac{1.1}{1.08}\right)^2$	-	1,037,940
Phase Three 26,330 × 36 ×	$\left(\frac{1.1}{1.08}\right)^4$	-	1,020,070
Annual Labour Costs (10% escala 60,000 × 40	ation)	-	2,400,000
Annual Maintenance Costs 1,700 × 40		-	68,000

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Replacement Costs

Year 20

$$24,000 \times \frac{1.1}{1.08}$$
 20

Year 25

 $162,000 \times \frac{1.1}{1.08}^{25}$

\$6,301,290

34,640

256,290

\$

LIFE CYCLE COST TWO - DIVERSE PLANT

Initial Costs Year One

1 x 3,000 MBH boiler		-	\$ 8,000
Gas vent	<u>*</u>);	-	2,000
Heating pump, 200 USGPM		-	1,000
1,000 4" heating pipe		-	16,000
1 400-ton chiller		-	60,000
1 100-ton reclaim condenser		-	10,000
Cooling tower, 400 ton		-	12,000
Chilled water pump, 480 USGPM		-	2,880
Condenser pump, 1,200 USGPM		-	6,000
1,000 5" chilled water pipe		-	20,000
360 Kw electrical distribution		-	10,800
Building enclosure		-	 10,000

\$ 158,680

Future Cost - Phase Two, Year Two (1975 dollars)

1 x 3,000 MBH boiler	-	\$	8,000
Gas vent	-		2,000
Heating pump, 200 USGPM			1,000
600 – 4" heating pipe	-		9,600
1×260 ton chiller	-		39,000
1 x 100 ton reclaim condenser			10,000
Cooling tower – 260 ton	-		7,800
Chilled water pump, 312 USGPM	-		1,860
Condenser water pump, 780 USGPM	-		3,900
600 – 5" chilled water pipe	-		12,000
250 Kw electrical distribution	-		7,500
Building enclosure	-	9.5	10,000

\$ 110,660

Future Cost - Phase Three, Year Four (1975 dollars)

1 300 MBH boiler	-	\$	8,000
Gas vent	_		2,000
			1,000
Heating pump, 200 USGPM	and a second		
300 ft. 4" heating pipe			4,800
1 260-ton chiller	-		39,000
1 100-ton reclaim condenser			10,000
Cooling tower – 260 ton			7,800
Chilled water pump, 312 USGPM	-		1,860
Condenser water pump, 780 USGPM	_		3,900
300 ft. 5" chilled water pipe			6,000
250 Kw electrical distribution	-		7,500
Building enclosure	-		10,000
		\$	101,860
		*	,
Annual Energy Costs (1975 dollars)			
Each Phase			
Cooling - \$18,360			
•	_	\$	26,330
Heating - <u>7,970</u>		φ	20,000
Annual Labour Costs (1975 dollars)			
Initial		¢	15 000
Three operators	-	\$	45,000
Year Three onward - four operators	_	\$	60,000
Tear Three onward Tour operators		4	,
Annual Maintenance Costs (1975 dollars)			
Year One			
Clean one boiler	-	\$	200
Clean one chiller	-		500
Otean one critter			
		¢	700
		\$	700
Year Two			
Clean two boilers	-	\$	400
Clean two chillers	-		900
		0.000	
		\$	1.,300
			,
Year Four			
Clean two boilers	-	\$	500
	100	4	
Clean two chillers			1,200
			1 800
		\$	1,700

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Replacement Costs (1975 dollars)		
Year 20 - Replace boiler Year 22 - Replace boiler Year 24 - Replace boiler Year 25 - Replace chiller Year 27 - Replace chiller Year 29 - Replace chiller		\$ 8,000 8,000 8,000 70,000 49,000 49,000
Thus the Life Cycle Cost, 30 years, with 8% P.D. Equipment:	.V. dis	scount – Diverse
Initial Costs	-	\$ 158,680
Future Costs - Phase Two (6% escalation) 110,660 × $\left(\frac{1.06}{1.08}\right)^2$ =	-	106,600
Future Costs - Phase Three (6% escalation) 101,860 × $\left(\frac{1.06}{1.08}\right)^2$ =	-	94,520
Annual Energy Costs (10% escalation)		
Phase One 26,330 × 40	-	1,053,200
Phase Two 26,330 × 38 × $\left(\frac{1.1}{1.08}\right)^2$	-	1,037,940
Phase Three 26,330 × 36 × $\left(\frac{1.1}{1.08}\right)^4$	-	1,020,070
Annual Labour Costs (10% escalation)		
First Two Years 45,000 x 2	-	\$ 90,000
After Two Years 60,000 × 38 × $\left(\frac{1.1}{1.08}\right)^2$	-	2,365,230

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Annual Maintenance Costs (10% escalation)	94	
Year One	-	\$ 700
Years Two and Three 1,300 × 2 × $\left(\frac{1.1}{1.08}\right)^2$	-	2,700
Year Four on 1,700 × 36 × $\left(\frac{1.1}{1.08}\right)^4$	-	<u>65,860</u> \$5,995,500
Replacement Costs (10% escalation)		
Year 20 8,000 × $\frac{(1.1)^{20}}{(1.08)^{20}}$	-	\$ 11,550
Year 22 8,000 $\times \frac{(1.1)^2}{(1.08)^{22}}$	-	12,000
Year 24 8,000 $\times \frac{(1.1)^{24}}{(1.08)^{24}}$	-	12,430
Year 25 70,000 × $\frac{(1.1)^{25}}{(1.08)^{25}}$	-	110,750
Year 27 49,000 × $\frac{(1.1)^{27}}{(1.08)^{27}}$	-	80,420
		\$6,222,650

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LIFE CYCLE COSTS - DIVERSE EQUIPMENT WITH STORAGE

Equipment Requirements	Coolir Tons	ng _	Heating MBH
Lakeshore Teacher's College	300		-
Phase One, New Construction	100		2,900
Phase Two, New Construction	-		2,900
Phase Three, New Construction	260		2,900
Initial Costs – Year One			
		¢	0.000
1 x 3,000 MBH boiler Gas vent	-	\$	8,000
Heating pump, 200 USGPM	_		2,000
1,000 ft. 4" heating pipe			1,000 16,000
1 - 400 ton chiller			60,000
1 – 200 ton reclaim condenser			20,000
Cooling tower, 400 ton	_		12,000
Chilled water pump, 480 USGPM	_		2,880
Condenser water pump, 1,200 USGPM	_		6,000
1,000 ft. 5" chilled water pipe	_		20,000
360 Kw electrical distribution	-		10,800
Building enclosure			10,000
Storage tank	-		141,000
		\$	309,680
Future Cost - Phase Two, Year Two			
1 300 MBH boiler	-	\$	8,000
Gas vent	-		2,000
Heating pump, 200 USGPM			1,000
600 ft. 4" heating pipe	-		9,600
1 260-ton chiller	-		39,000
1 100-ton reclaim condenser	-		10,000
Cooling tower, 260 ton	_		7,800
Chilled water pump, 312 USGPM	3 .		1,860
Condenser water pump, 780 USGPM	-		3,900
600 ft. 5" chilled water pipe	-		12,000
250 Kw electrical distribution	-		7,500
Building enclosure	-	-	10,000

112,660

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Future Cost - Phase Three, Year Four		
1 x 3,000 MBH boiler Gas vent Heating pump 300 ft. 4" heating pipe Chilled water pump 30 Kw electrical distribution Building enclosure		\$ 8,000 2,000 1,000 4,800 1,860 900 2,500
		\$ 21,060
Annual Energy Costs (1975 dollars)		
Years One and Two Cooling Heating	-	\$ 13,020 4,190
		\$ 17,210
Years Three and Four Cooling Heating	-	\$ 31,380 12,160
		\$ 43,540
Year Five on		
Cooling Heating	-	\$ 49,740 20,130
	8	\$ 69,870
Annual Labour Costs (1975 dollars)		
Initial Three operators	-	\$ 45,000
Year Three onward Four operators	-	60,000
Annual Maintenance Costs (1975 dollars)		(9)
Year One Years Two and Three Year Four on	Ē	\$ 700 1,300 1,400

ENGINEERING INPEREACE LIMPER)

Replacement Costs (1975 dollars)

Year 20	Replace boiler	-	\$ 8,000
Year 22	Replace boiler		8,000
Year 24	Replace boiler	-	8,000
Year 25	Replace chiller	-	70,000
Year 27	Replace chiller	-	49,000

Life Cycle Cost - 30 years, 8% P.D.V. Discount for Diverse Plant with Thermal Storage

Initial Costs	-	\$ 309,680
Future Costs, Phase Two (6% escalation)		κ.
112,660 × $\frac{(1+0.06)^2}{(1+0.08)^2}$	-	108,530

Future Costs, Phase Three (6% escalation) $21,060 \times \frac{(1.06)^4}{(1.08)^4}$ - 19,540

Annual Energy Costs (10% escalation)

Years Three and Four

$$43,540 \times 2 \times \frac{(1.1)^2}{(1.08)^2} - 90,335$$

Year Five on $69,870 \times 35 \times \frac{(1.1)^4}{(1.08)^4}$ - 2,445,450

Annual Labour Costs (10% escalation)

Years One and Two 45,000 x 2 - 90,000

Year Three on

$$60,000 \times 38 \times \frac{(1.1)^2}{(1.08)^2} - 2,365,230$$
C/F \$5,463,185

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	B/F	\$5,463,185
Annual Maintenance Costs (10% escalation)		
Years One and Two	-	700
Years Two and Three $1,300 \times 2 \times \frac{(1.1)^2}{(1.08)^2}$	-	2,700
Year Four on 1,400 × 36 × $\frac{(1.1)^4}{(1.08)^4}$	-	54,240
Replacement Costs (10% escalation)		
Year 20 8,000 × $\frac{(1.1)^{20}}{(1.08)^{20}}$	-	11,550
Year 22 8,000 × $\frac{(1.1)^{22}}{(1.08)^{22}}$	-	12,000
Year 24 8,000 × $\frac{(1.1)^{24}}{(1.08)^{24}}$	-	12,430
Year 25 70,000 × $\frac{(1.1)^{25}}{(1.08)^{25}}$	-	110,750
Year 27 49,000 × $\frac{(1.1)^{27}}{(1.08)^{27}}$	-	80,420 \$ 5,747,975
In summary, the life cycle costs are:		
 Central Equipment Diverse Equipment Diverse Equipment with Storage 		\$ 6,301,290 \$ 6,222,650 \$ 5,747,975

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ENGINEERING INPEREACE LIMPED

Thus, despite high initial expenditure, thermal storage shows considerable saving over the life cycle.

CONCLUSIONS

Presuming the final design closely follows the building used in this analysis, the following are recommended system approaches:

- Diverse equipment.
- Heat pump reclaim for two phases.
- Thermal storage for one phase.
- Pilot solar collector, first phase.
- Waste incineration, if suitable rebate can be obtained for energy saved.
- Gas boilers.
- Radiation at perimeter sized for low temperature water of heat reclaim cycle. Individual control on rooms subject to direct solar gain.
- Variable air volume systems with economizer cycles modulated to ensure heat reclaim.

PROJECT COSTS

Using these conclusions as a basis for design, the estimated budget costs for each phase of construction, based on first quarter 1975 dollars, are as follows:

First Phase, New Construction

Heating, Ventilating and Air Conditioning Plumbing, Drainage and Fire Protection	-	\$ 840,000 \$ 375,000
Second Phase, New Construction		
Heating, Ventilating and Air Conditioning		
including Storage Tank	<u> </u>	\$ 850,000
Plumbing, Drainage and Fire Protection	-	\$ 245,000

-

Heating, V	entilating and Air Conditioning	-	\$ 750,000
	Drainage and Fire Protection		\$ 245,000

Cost Appendix

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Adjacent Site: View to Lake Ontario

	Element	Amount \$	Total Cost \$	Rate \$/SF Floor Area		%	Comments
1Substructure(a)Normal foundations(b)Basement excavations(c)Special conditions	91,360 	116,750	0.57	0.73	2.2		
(a)	Structure Lowest floor construction Upper floor construction Roof construction	96,790 473,000 296,000	865,790	0.61 2.97 1.86	5.44	16.4	
3 (a) (b) (c) (d) (e) (f)	Exterior Cladding Roof finish Walls below ground floor Walls above ground floor Windows Exterior doors & screens Balconies & projections	258,000 - 447,480 114,000 10,000 15,000	844,480	1.62 - 2.82 0.72 0.06 0.09	5.31	16.0	
4 (a) (b) (c)	Interior Partitions Permanent partitions Movable partitions Doors	204,170 2,500 97,940	304,610	1.28 0.02 0.62	1.92	5.8	
5 (a) b)	Vertical Movement Stairs Elevators & escalators	30,000 48,000	78,000	0.19 0.30	0.49	1.5	
a) b)	Interior Finishes Floor finishes Ceiling finishes Wall finishes	119,250 79,500 83,100	281,850	0.75 0.50 0.52	1.77	5.3	
7 (a) b)	Fittings & Equipment Fittings & fixtures Equipment	119,250 119,250	238,500	0.75	1.50	4.5	· .

Hanscomb Roy Associates Elemental Cost Summary Part 1 of 2

Project: HUMBER - LAKESHORE CA	MPUS – PHAS			ary Estin ne 18, 19		Sheet No: A.2
Element	Amount \$	Total Cost \$	Rate Floor		%	Comments
 8 Services (a) Electrical (b) Plumbing & drainage (c) Heating, ventilation & air conditioning 	850,000 375,000 840,000	2,065,000	5.34 2.36 5.29	12.99	39.2	•
9 Overheads & Profit		479,500		3.02	[.] 9.1	10% of 4,794,980
Net Building Cost		5,274,480		33.17	100	
10Site Development(a)General(b)M & E site services(c)Alterations(d)Demolition	334,950 203,500 - -	538,450	2.11 1.28 -	3.39		including contingencies
11 Contingencies		527,450		3.32		10% of NBC
12 Link to L.T.C.		250,000		1.57		Allowance
F.S.T. Rebate		6,590,380 (89,110) <u>6,501,270</u>		41.45 (0.56) <u>40.89</u>		Gross Floor Area 159,000 G 1.25% of all but element 10
Net Building Cost 33.17 Contingencies 3.32 F.S.T. Rebate (0.56) \$35.93/GSF						** ** /*

Element	Amount \$ 75,780 19,620	Total Cost \$ 95,400	Rate \$/SF Floor Area		%	Comments
 Substructure a) Normal foundations b) Basement excavations c) Special conditions 			0.48	0.61	2.0	
 2 Structure a) Lowest floor construction b) Upper floor construction c) Roof construction 	66,120 559,900 246,820	872,840	0.42 3.57 1.57	5.56	18.0	
 3 Exterior Cladding a) Roof finish b) Walls below ground floor c) Walls above ground floor d) Windows e) Exterior doors & screens f) Balconies & projections 	98,560 	546,960	0.63 - 2.14 0.43 0.06 0.22	3.48	11.3	
 4 Interior Partitions a) Permanent partitions b) Movable partitions c) Doors 	196,560 2,500 120,580	319,640	1.25 0.02 0.77	2.04	6.6	
5 Vertical Movement a) Stairs b) Elevators & escalators	22,500 27,000	49,500	0.15 0.17	0.32	1.0	
 6 Interior Finishes a) Floor finishes b) Ceiling finishes c) Wall finishes 	157,000 78,500 104,120	339,620	1.00 0.50 0.66	2.16	7.0	
7 Fittings & Equipment a) Fittings & fixtures b) Equipment	117,750 157,000	274,750	0.75	1.75	5.7	

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Hanscomb Roy Associates Elemental Cost Summary Part 1 of 2

Project:HUMBER - LAKESHORE CAMPUS - PHASE IIPreliminary EstimateSheetDate:June 18, 1975No: A.4							
Element	Amount \$	Total Cost \$	Rate Floor		%	Comments	
 8 Services (a) Electrical (b) Plumbing & drainage (c) Heating, ventilation & air conditioning 	805,000 245,000 850,000	1,900,000	5.13 1.56 5.41	12.10	39.3		
9 Overheads & Profit		439,870		2.80	9.1	10% of 4,398,710	
Net Building Cost		4,838,580		30.82	100		
10Site Development(a)General(b)M & E site services(c)Alterations(d)Demolition	499,730 108,900 -	608,630	3.18 0.69 - -	3.87		including contingencies	
11 Contingencies		483,870		3.08		10% of NBC	
		5,931,080		37.77		Gross Floor Area: 157,000 S	
Federal Sales Tax Rebate		(74,140)		(0.47)		1.25% of all but element 10	
		5,856,940		37.30		9.	
Net Building Cost 30.82 Contingency 3.08 F.S.T. Rebate (0.47) \$33.43 /GSF							
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	Element	Amount \$	Total Cost \$	Rate S Floor		%	Comments
1 (a) (b) (c)	Substructure Normal foundations Basement excavations Special conditions	74,200	98,630	0.53	0.70	2.1	
2 (a) (b) (c)	Structure Lowest floor construction Upper floor construction Roof construction	89,400 382,250 295,390	767,040	0.64 2.72 2.10	5.46	16.4	
3 (a) (b) (c) (d) (e) (f)	Exterior Cladding Roof finish Walls below ground floor Walls above ground floor Windows Exterior doors & screens Balconies & projections	542,940 - 179,320 38,160 10,000 29,800	800,220	3.87 1.28 0.27 0.07 0.21	5.70	17.0	
4 (a) b) (c)	Interior Partitions Permanent partitions Movable partitions Doors	180,690 2,500 86,490	269,680	1.29 0.02 0.61	1.92	5.8	
5 (a) b)	Vertical Movement Stairs Elevators & escalators	15,000 18,000	33,000	0.11 0.13	0.23	0.7	
a) b)	Interior Finishes Floor finishes Ceiling finishes Wall finishes	140,400 70,200 96,440	307,040	1.00 0.50 0.69	2.19	6.6	
7 a) b)	Fittings & Equipment Fittings & fixtures Equipment	105,300 70,000	175,300	0.75	1.25	3.7	

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Elemental Cost Summary Part 1 of 2

	Element	Amount \$	Total Cost \$	Rate Floor	\$/SF Area	%	Comments
8 (a) (b) (c)	Services Electrical Plumbing & drainage Heating, ventilation & air conditioning	805,000 245,000 750,000	1,800,000	5.73 1.75 5.34	12.82	38.4	
9	Overheads & Profit		425,100		3.03	9.3	10% of 4,250,910
	Net Building Cost		4,676,010		33.30	100	
10 (a) (b) (c) (d)	Site Development General M & E site services Alterations Demolition	366,080 88,000 - -	454,080	2.60 0.63 -	3.23		including contingencies
11	Contingencies		467,610		3.33		10% of NBC
	Federal Sales Tax Rebate		5,597,700 (64,300) 5,533,400		39.86 <u>(0.46</u>) <u>39.40</u>		Gross Floor Area: 140,400 SI
	Net Building Cost 33.30 Contingencies 3.33 F.S.T. Rebate (0.46) \$36.17/GSF		-				

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